

Degradation behavior of PEMFC

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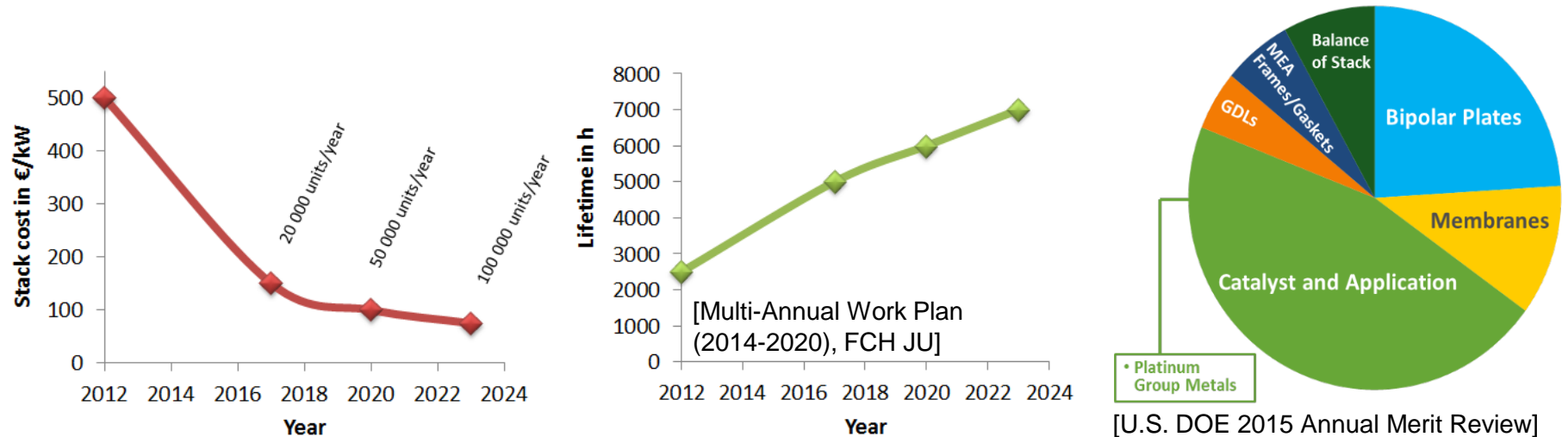
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Requirements for PEMFC development

- Reduction of manufacturing cost at increased durability in order to compete with conventional technologies



- Most promising regarding cost reduction: catalyst layer (45 % of stack cost)
 - **Low loadings**
 - Alternative catalysts



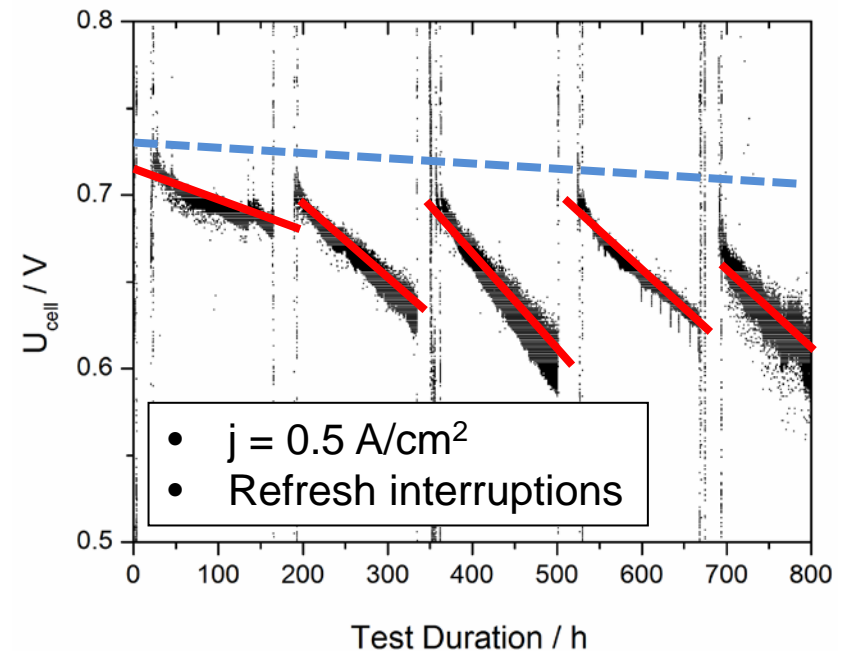
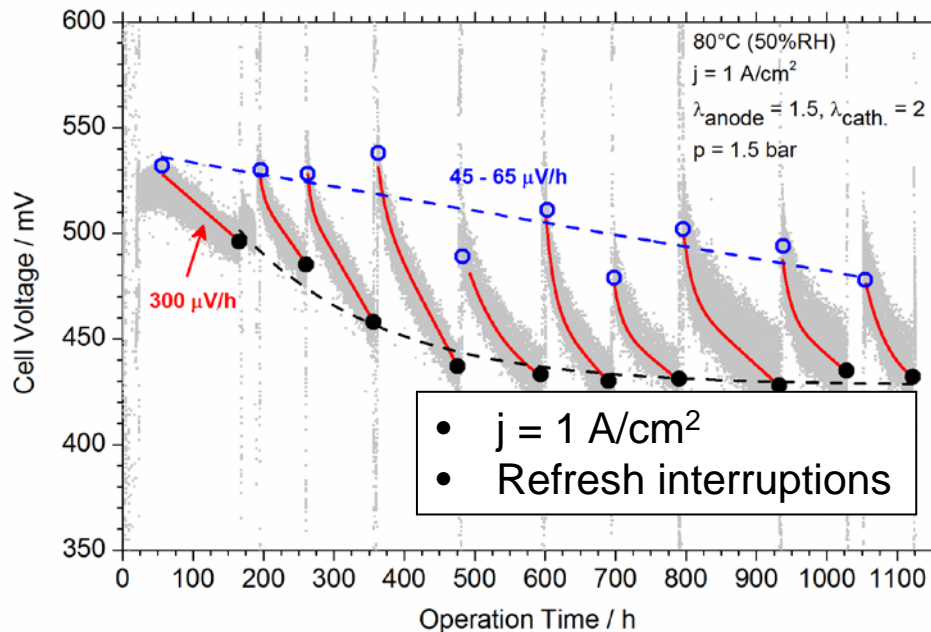
Motivation

Performance targets clearly defined and well verifiable, BUT

determination of **degradation rates** is not well defined.

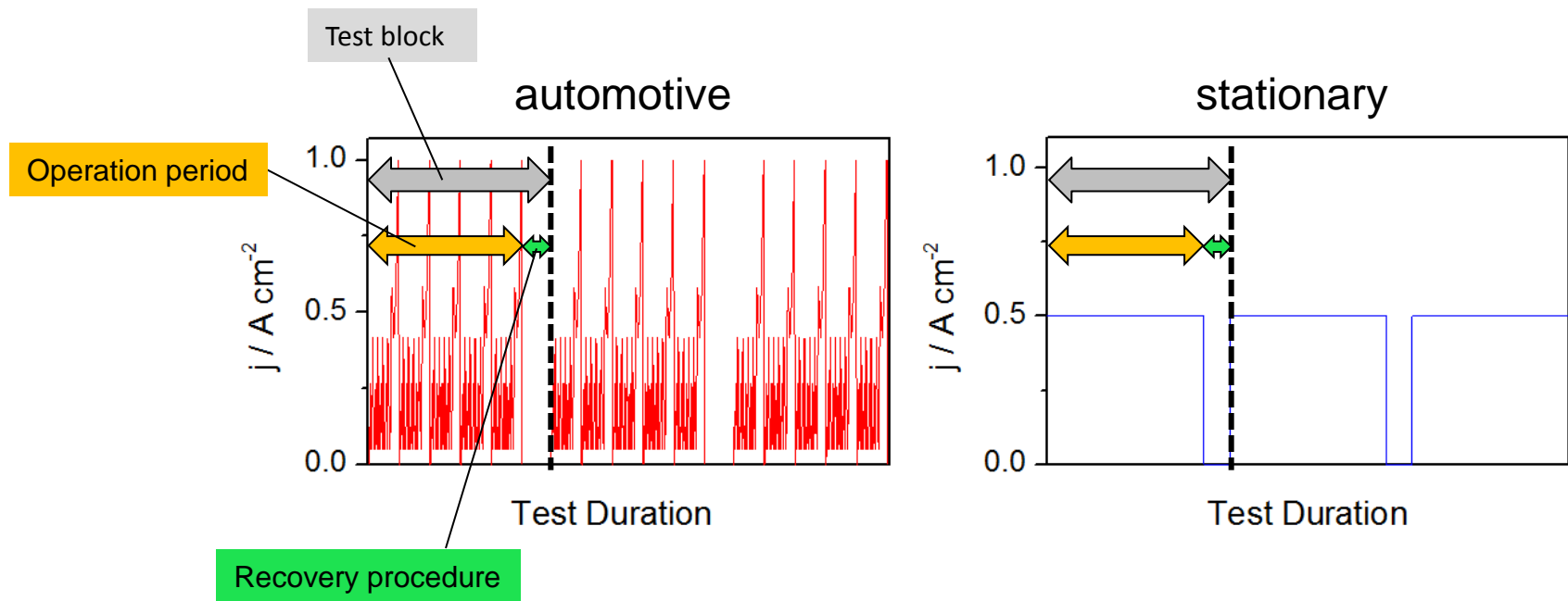
→ How to determine if **durability goals** are achieved?

Discrimination between **reversible** and **irreversible** degradation needed



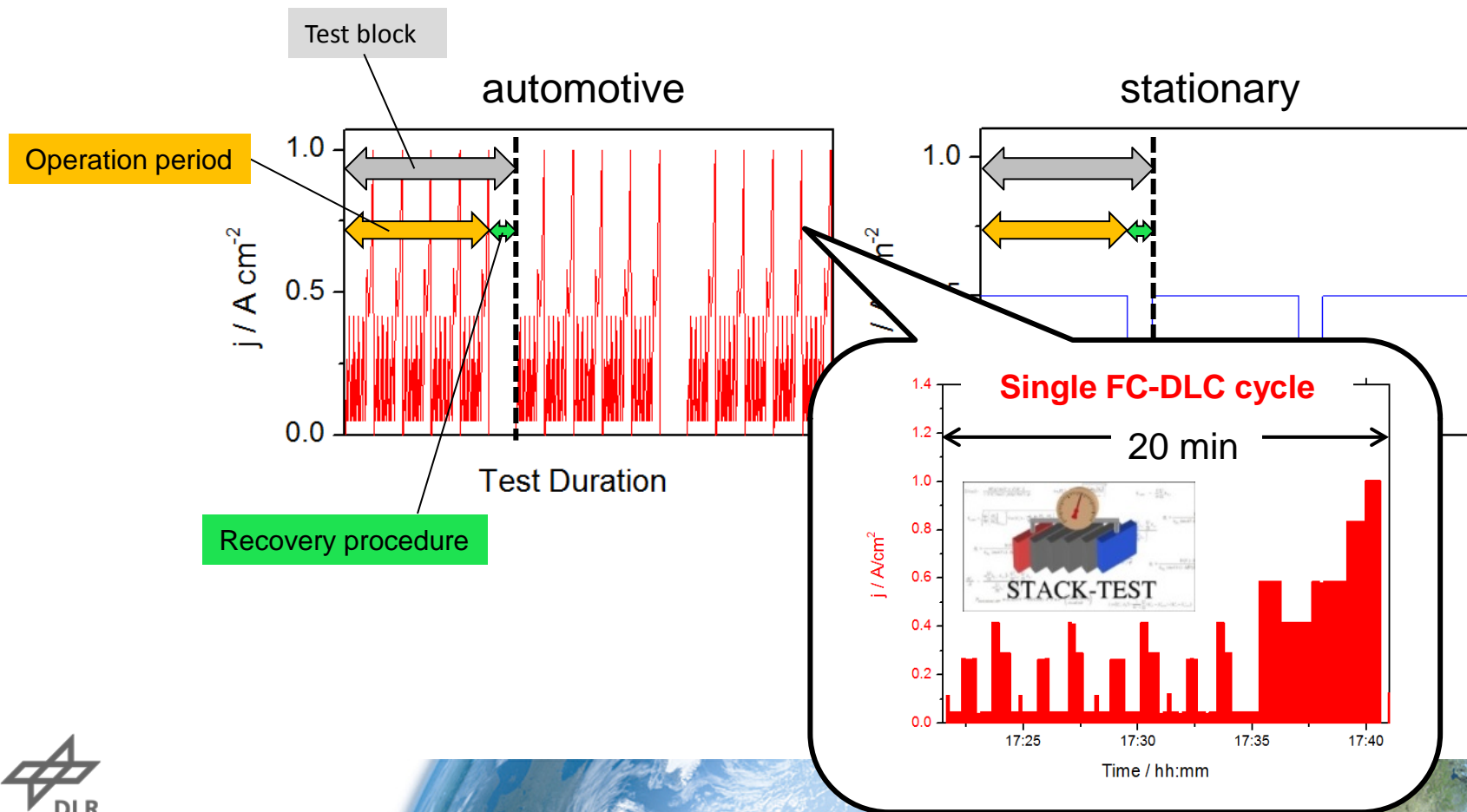
Evaluation of irreversible degradation

Durability tests consist of several test blocks of an **operation period** and a **recovery procedure**



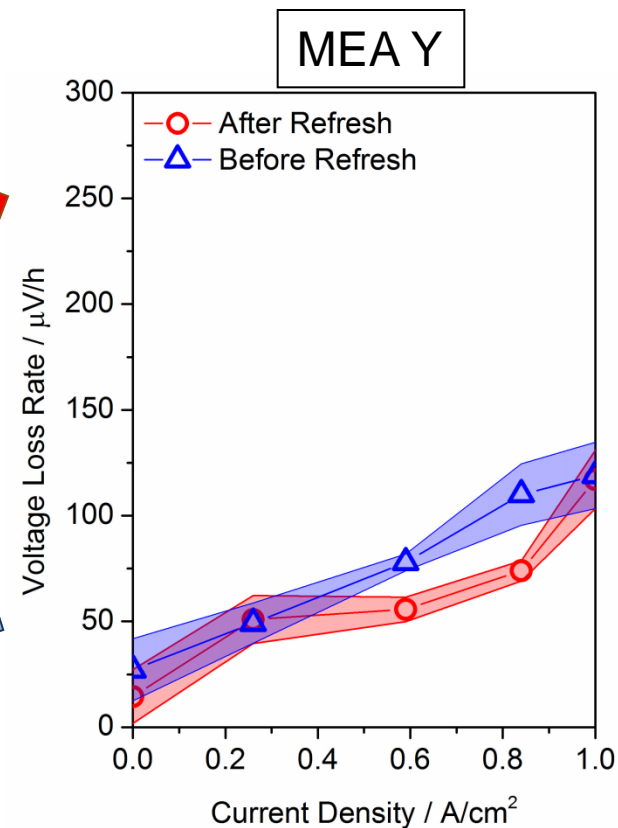
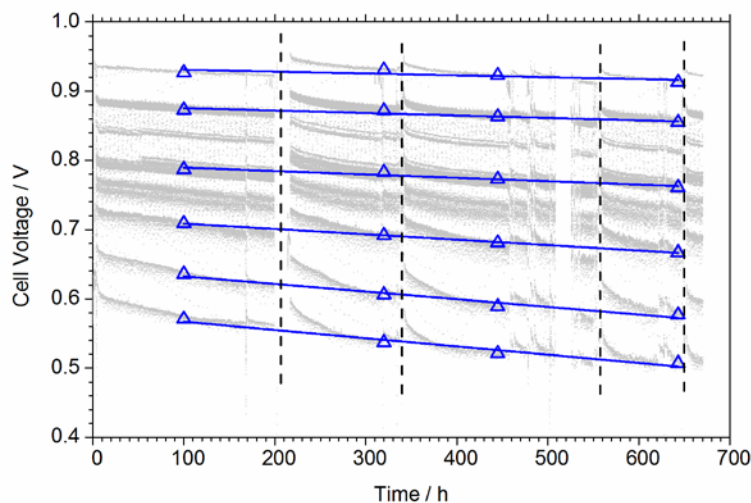
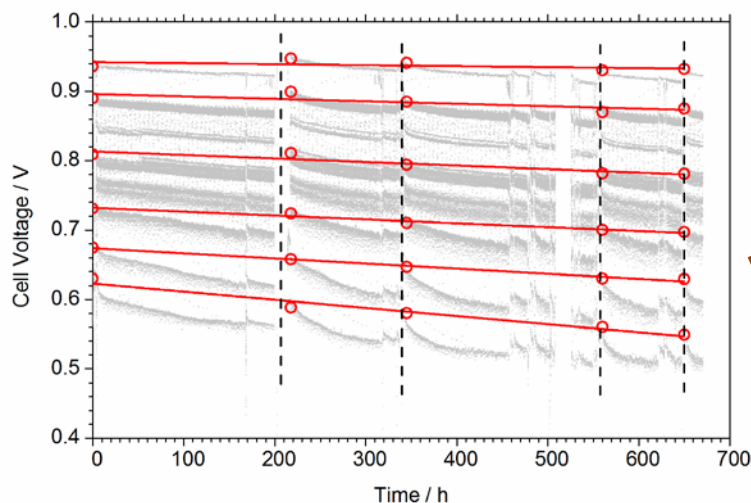
Evaluation of irreversible degradation

Durability tests consist of several test blocks of an **operation period** and a **recovery procedure**

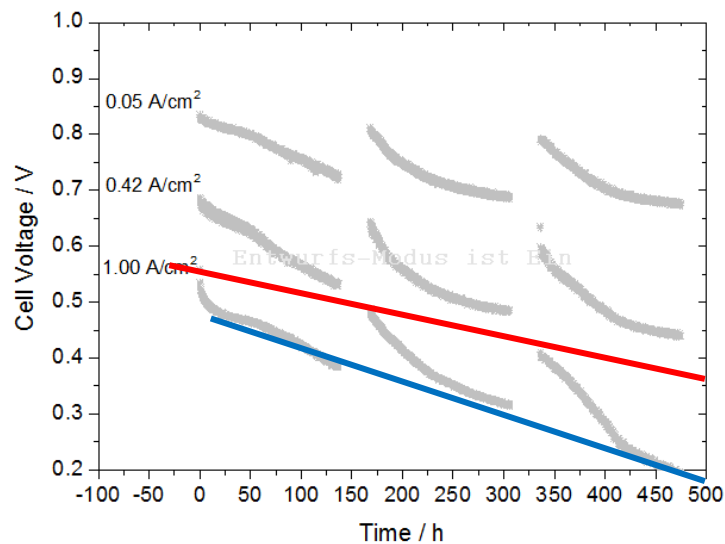


Evaluation of irreversible degradation

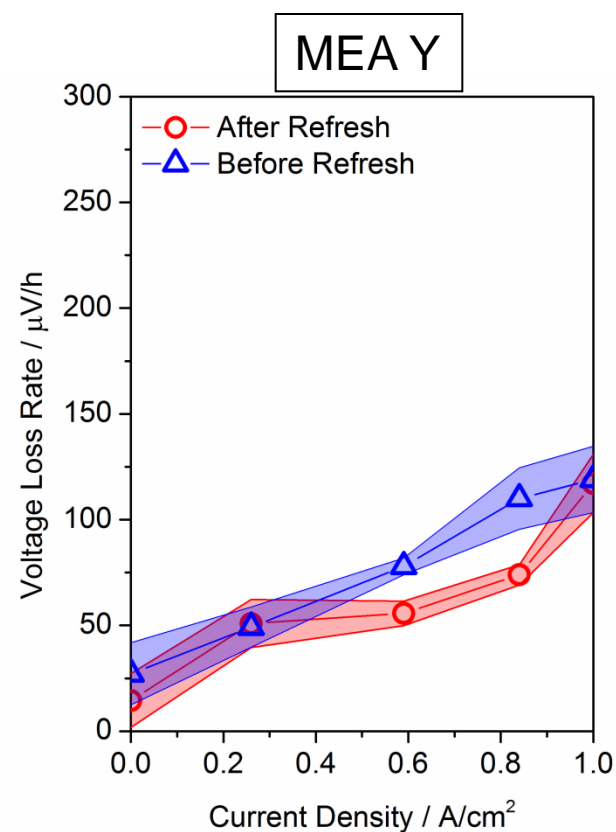
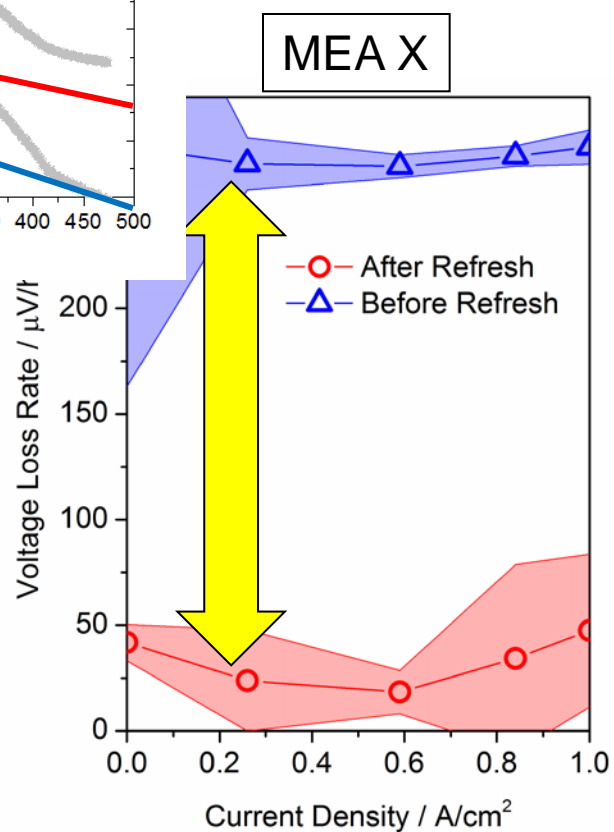
Use voltage values before or after refresh?



Evaluation of irreversible degradation



Use voltage values before or after refresh?

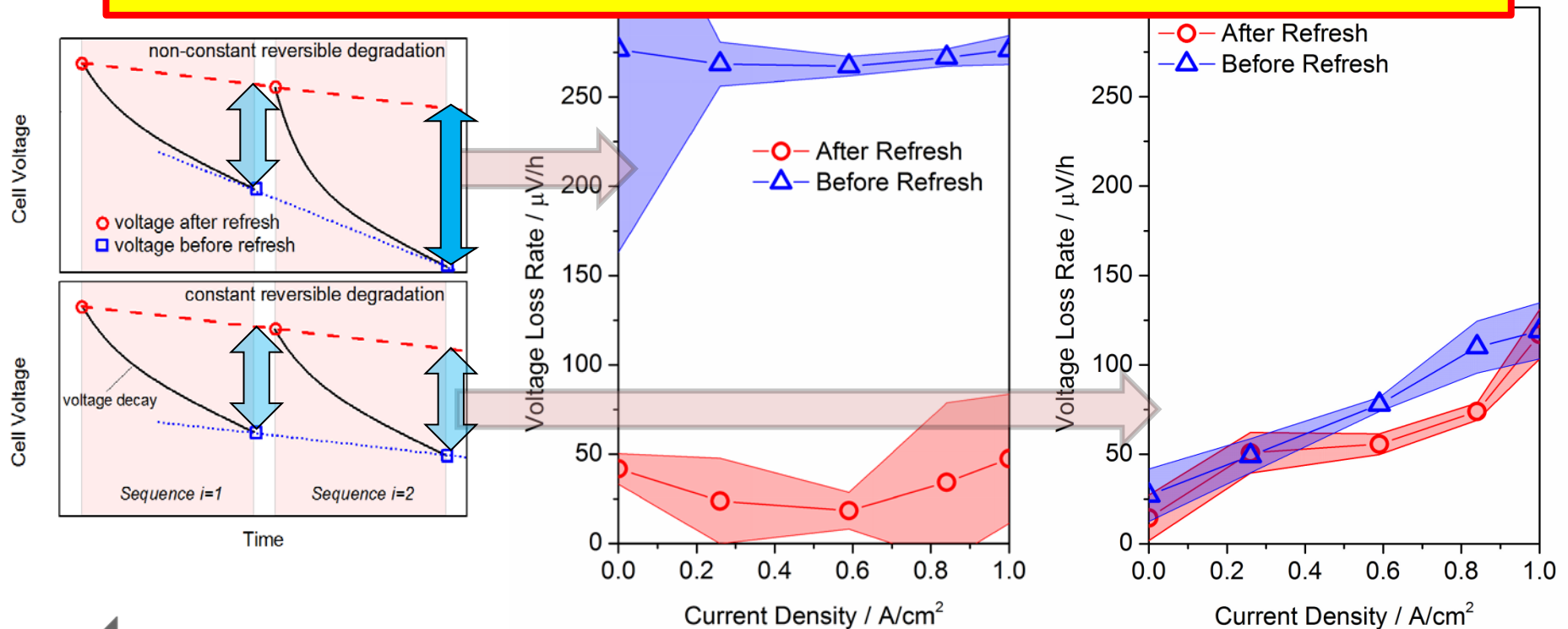


Evaluation of irreversible degradation

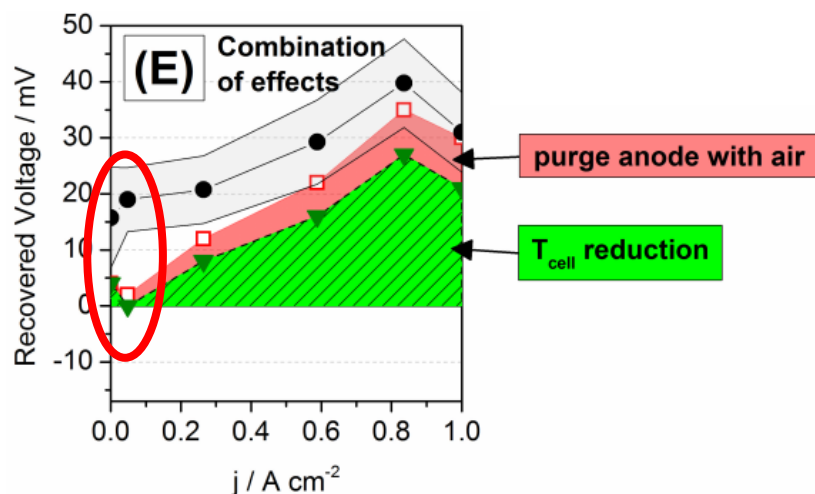
Constant and non-constant reversible degradation

→ decay rate(...): combination of **reversible** and **irreversible** degradation

→ decay rate(---): **irreversible** degradation



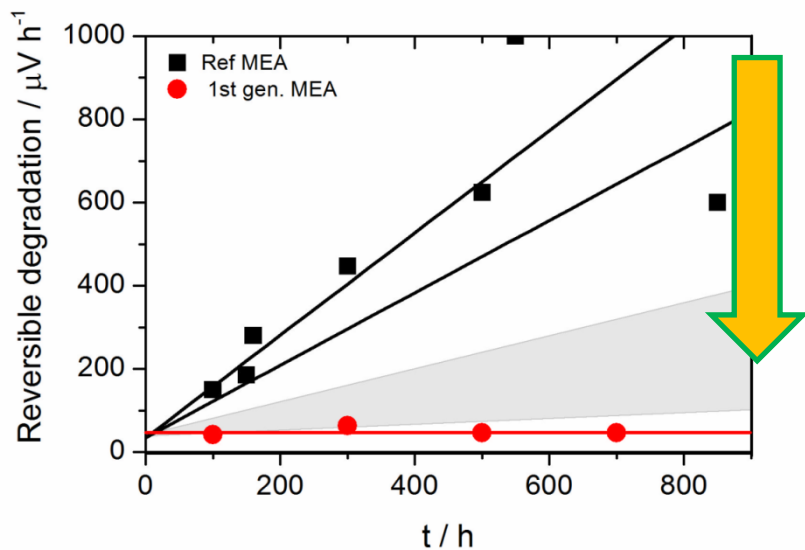
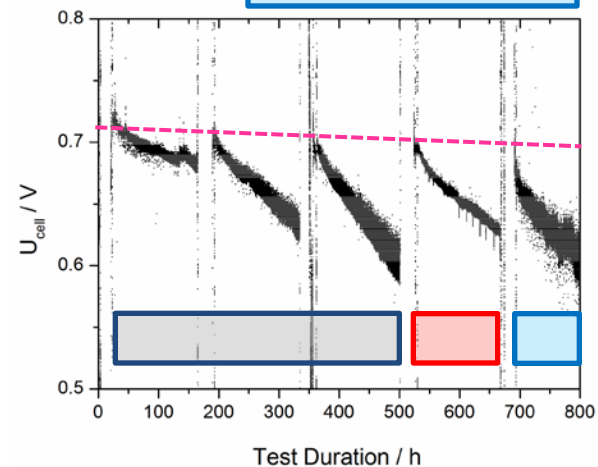
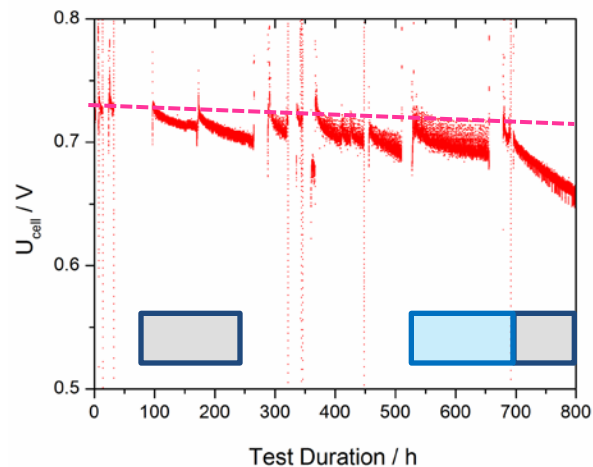
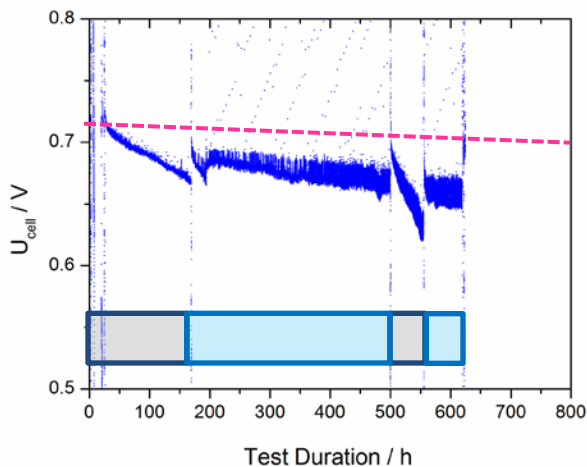
Recovery of reversible degradation



Recovery test	Intention	Recovered voltage @ 0.2 A cm^{-2}	Recovered voltage @ 0.8 A cm^{-2}
Purging anode with dry H_2	Remove water from anode	-28 %	-20 %
Purging cathode with dry air	Remove water from cathode	19 %	-10 %
Reduction of cell temperature	Increase humidity and decrease mechanical membrane stress	38 %	68 %
OCV-Test	Drying of MEA and increase of cathode potential	0 %	0 %
Purging anode with air	Increase anode potential to remove contaminants	19 %	20 %
Stopping gas flow	Increase anode potential to remove contaminants	0 %	10 %
Purging cathode with N_2	Decrease cathode potential to reduce platinum oxide	14 %	21 %

- Water management plays major role in recovery
- Reason for recovery at low loads unclear

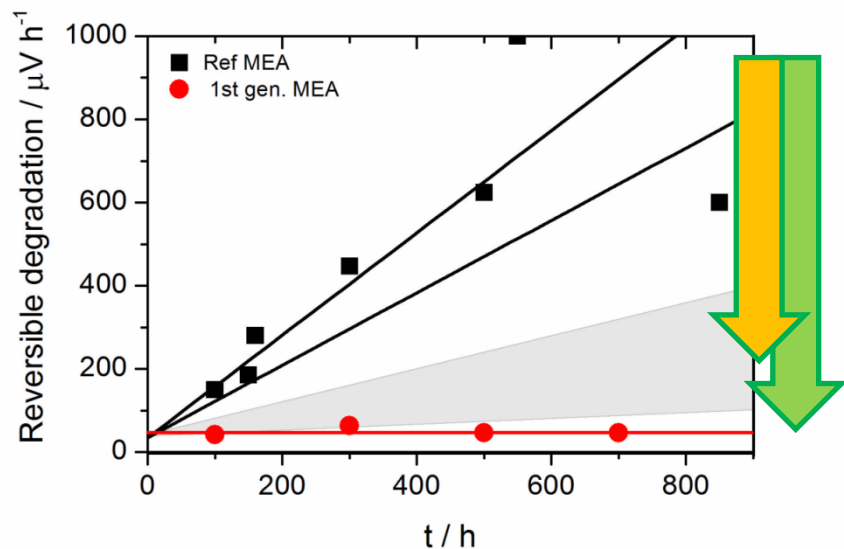
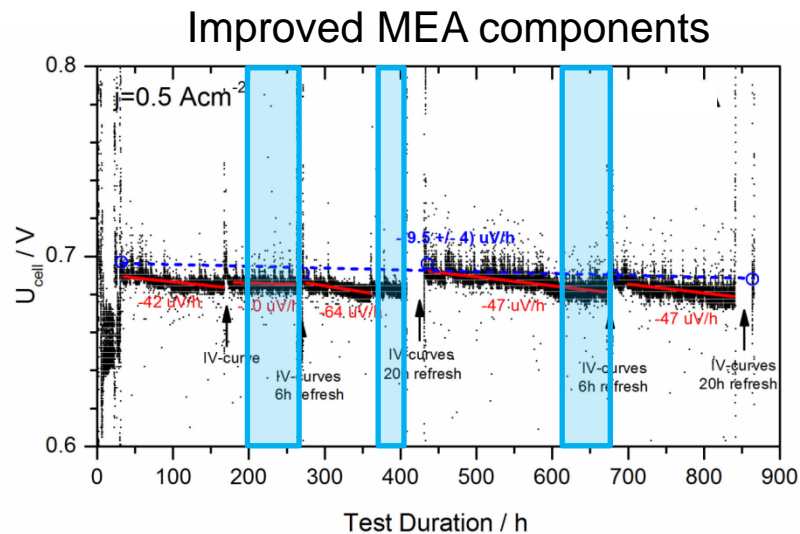
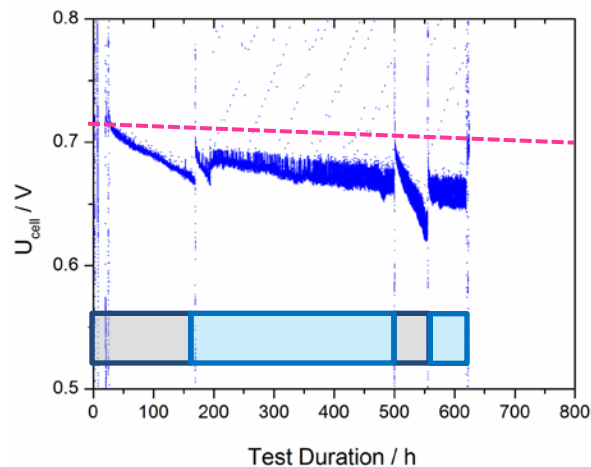
Reversible degradation



- Reversible degradation very sensitive to operation conditions
 → mitigation by e.g. OCV transient



Reversible degradation

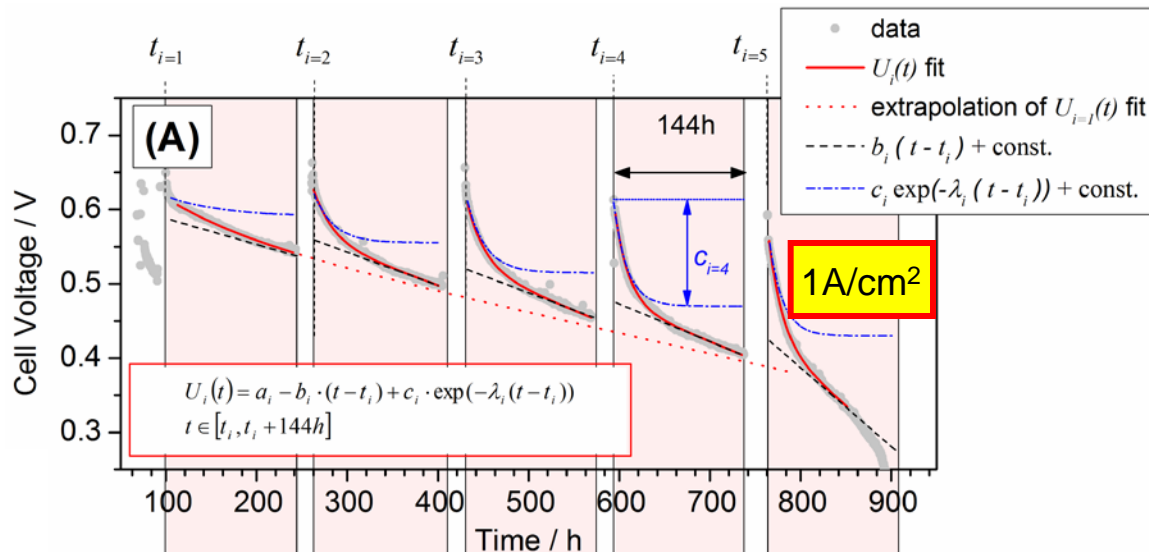


- Reversible degradation very sensitive to operation conditions
→ mitigation by e.g. OCV transient
- Mitigation by MEA modification

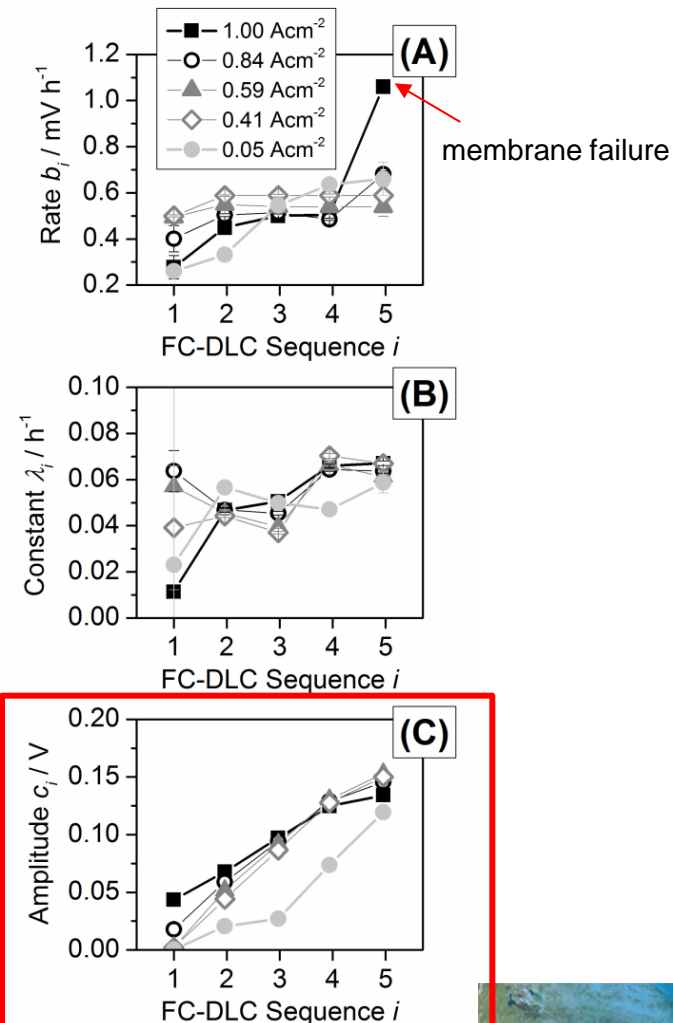


Evaluation of reversible degradation

Mathematical description of reversible degradation



Amplitude of exp. part responsible for increase of reversible degradation with operation time



Pt-Loading Rainbow Stack Study

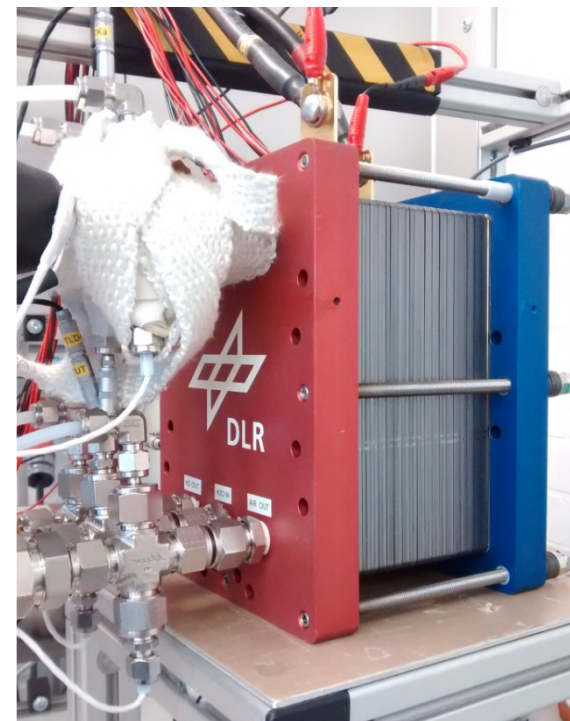
Pt-loadings at anode/cathode in $\text{mg}_{\text{Pt}}/\text{cm}^2$

1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19
MEA0476	MEA0476	MEA0476	0.05/0.20	0.05/0.30	0.05/0.40	0.05/0.15	0.10/0.40	0.20/0.40	MEA0476	0.05/0.20	0.05/0.30	0.05/0.40	0.05/0.15	0.10/0.40	0.20/0.40	MEA0476	MEA0476	MEA0476

Different Pt loadings

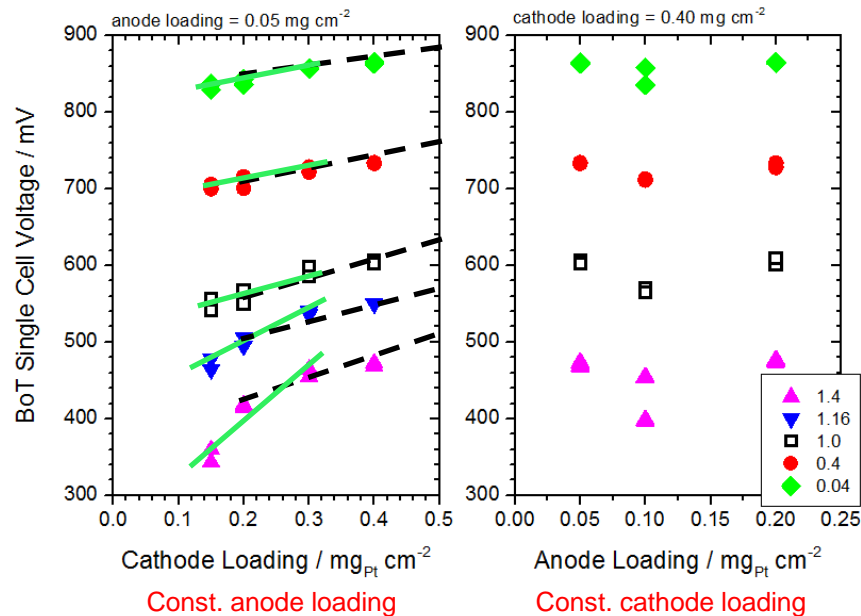
Different Pt loadings

DLR Rainbow-Stack



Performance Vs Pt-loading

BoT Voltages versus Loading

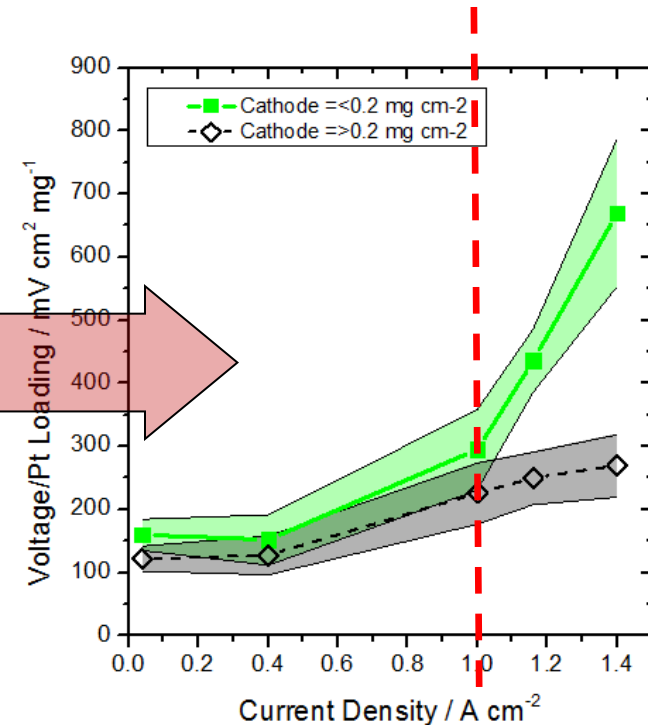
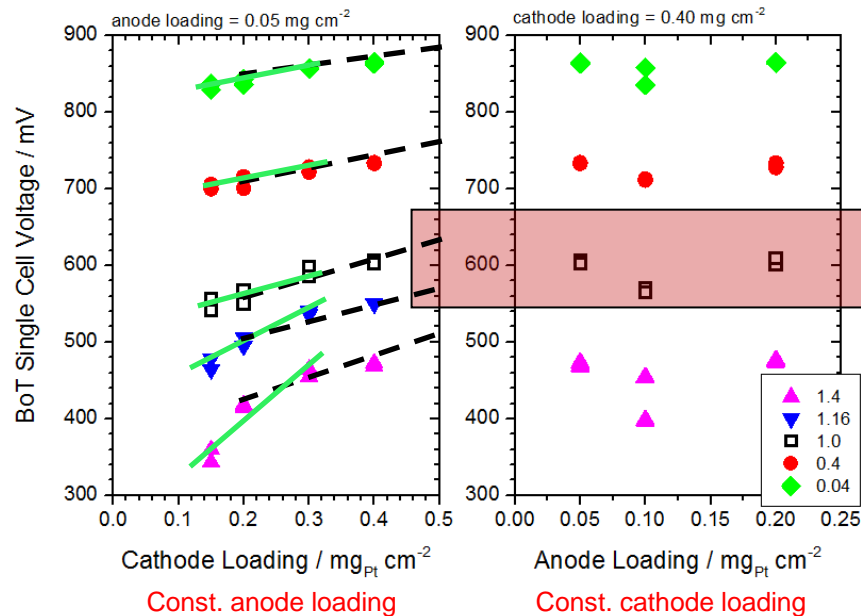


- Clear dependence of Cell Voltage on cathode Pt loading
- No dependence of Cell Voltage on anode Pt loading



Performance Vs Pt-loading

BoT Voltages versus Loading

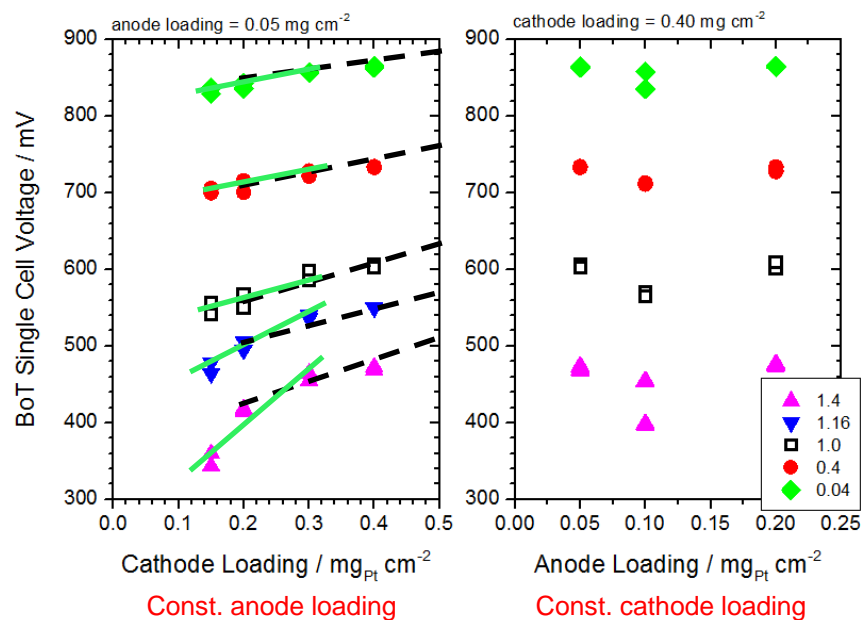


- Clear dependence of Cell Voltage on cathode Pt loading
- No dependence of Cell Voltage on anode Pt loading
- Onset of mass transport issues observed at cathode loading ≤ 0.2 mg/cm² and j > 1 A/cm²

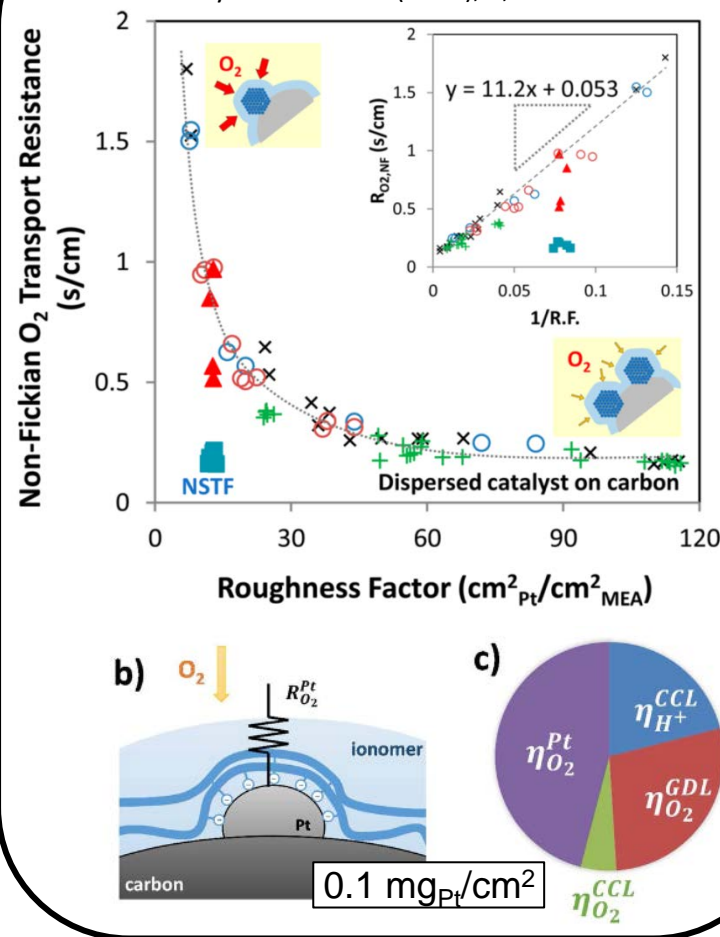


Performance Vs Pt-loading

BoT Voltages versus Loading



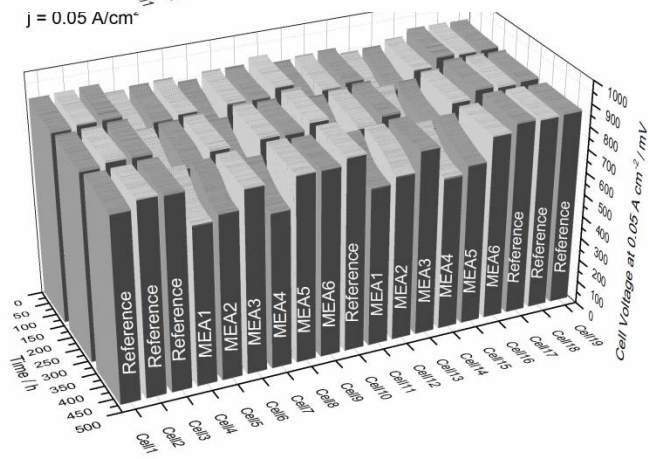
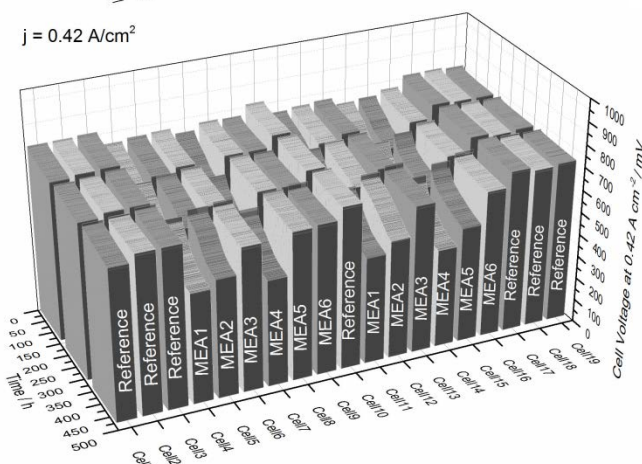
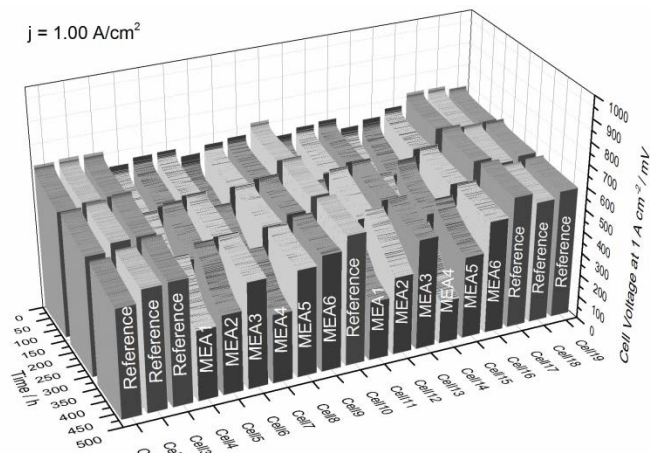
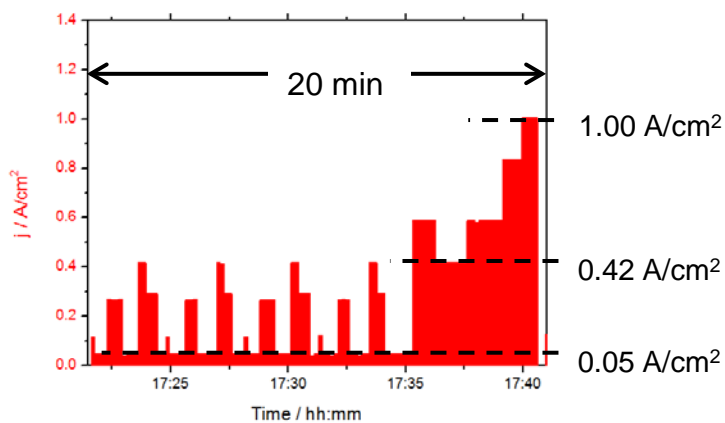
SOURCE: A. Kongkand and M.F. Mathias, J. Phys. Chem. Lett. (2016), 7, 1127



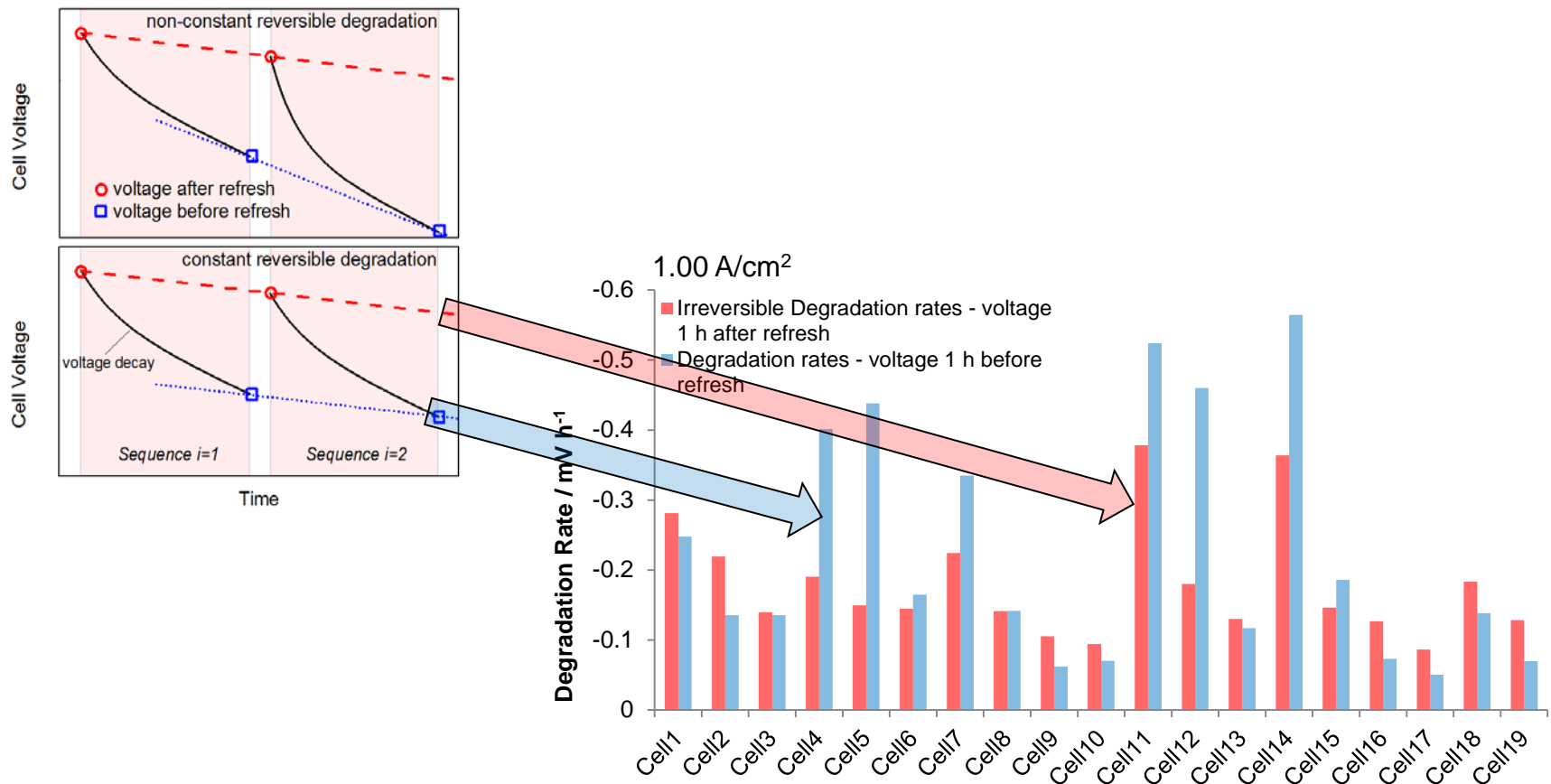
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Degradation Vs Pt-loading

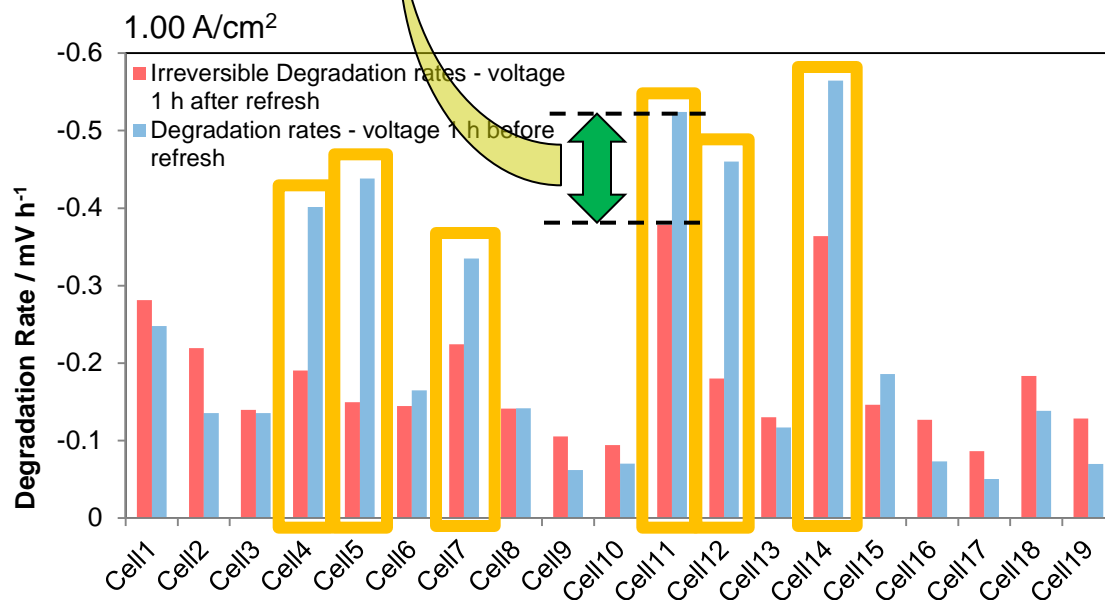
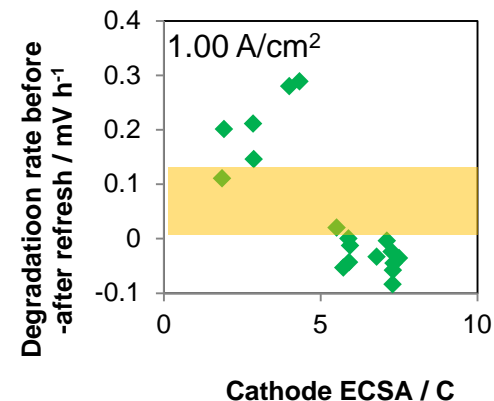
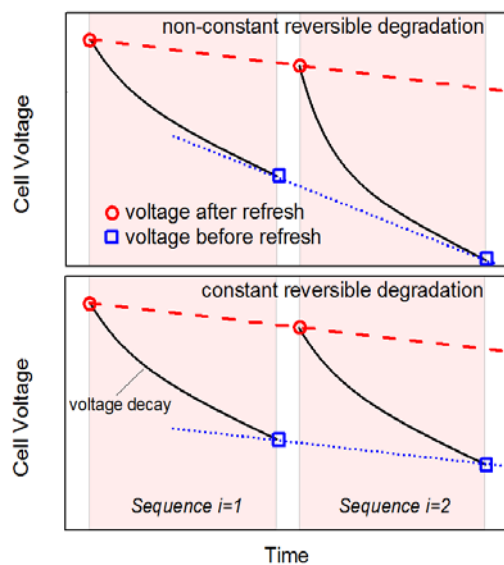
~500 h FC-DLC degradation test



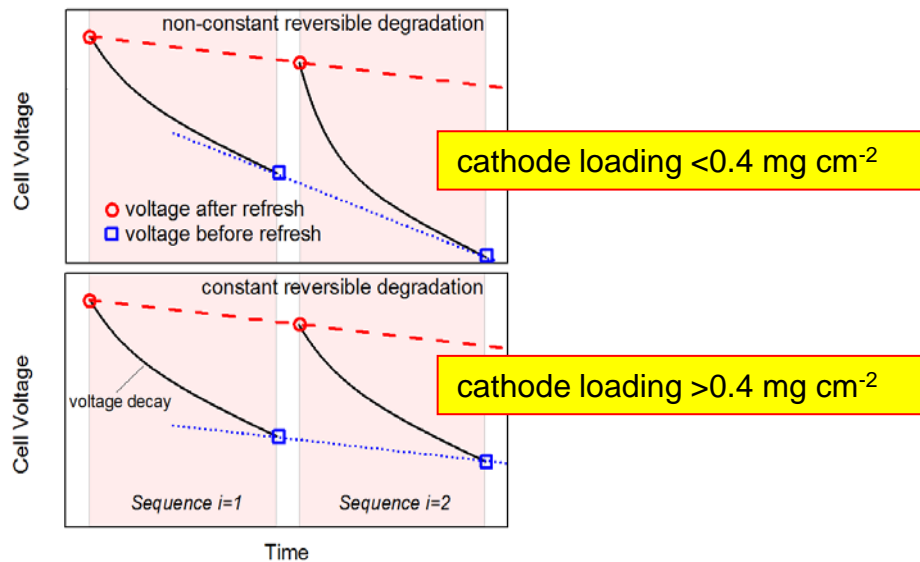
Degradation Vs Pt-loading: evaluation of rev. degradation



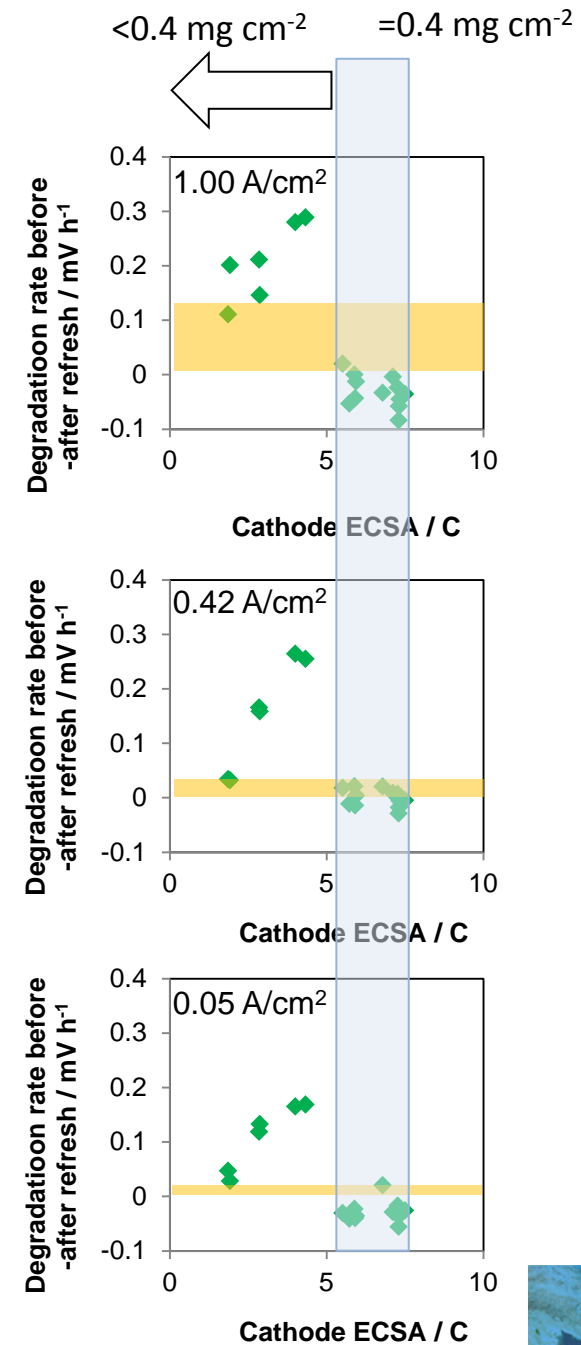
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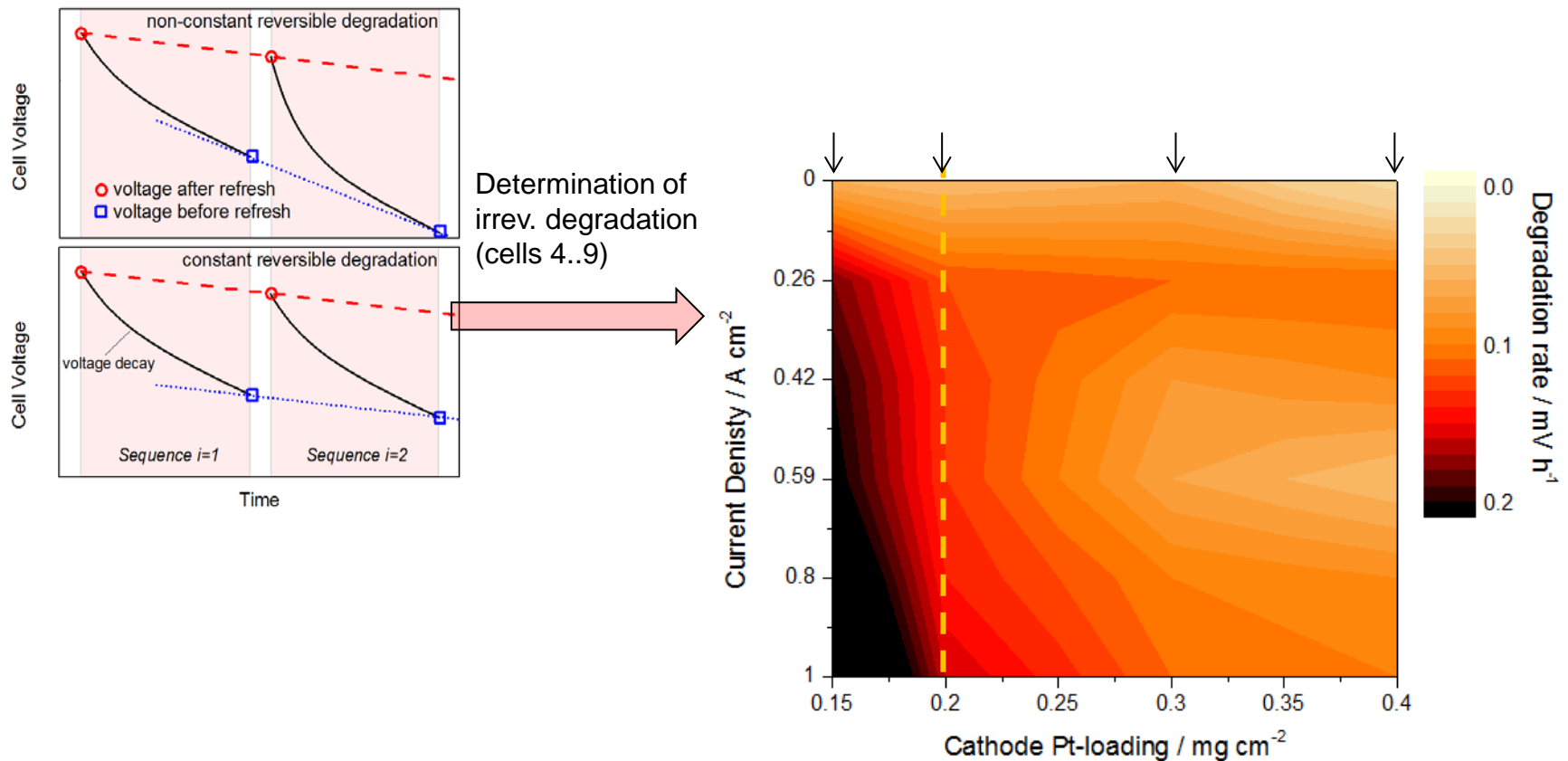


- MEAs with cathode loading $< 0.4 \text{ mg cm}^{-2}$ exhibit non-constant reversible degradation
- Effect strongest at high current density



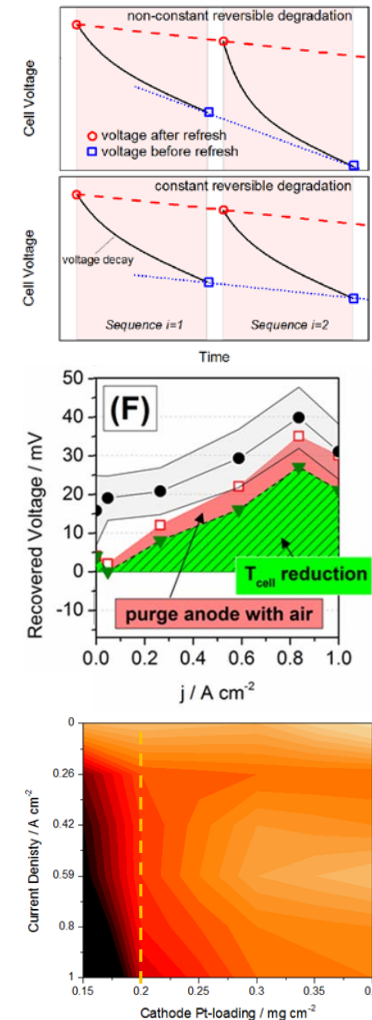
Degradation Vs Pt-loading: evaluation of irrev. degradation

Significant increase of irrev. degradation for cathode loading $< 0.2 \text{ mg/cm}^2$ and high loads



Summary

- Irreversible degradation rate: linear regression of voltage values after refresh
- Voltage recovery: water management, removal of anodic contaminants
- Degradation Vs Pt-loading:
 - accelerated rev. degradation for cathode loadings $< 0.4 \text{ mg cm}^{-2}$
 - increased irrev. degradation for cathode loading $< 0.2 \text{ mg cm}^{-2}$



Acknowledgements

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